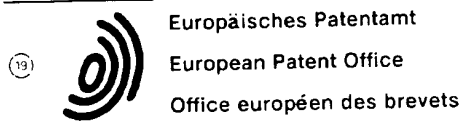


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Process for the activation of a catalyst.

A Fischer-Tropsch catalyst is activated by a process comprising reducing the catalyst by contact with a hydrogen-containing gas, the hydrogen concentration and the space velocity of the gas contacting the catalyst increasing step-wise or continuously during the activation. The process may be employed to activate a fresh catalyst prior to its use or to regenerate an exhausted or partially exhausted catalyst. The catalyst, once activated, may be used in a process for the preparation of hydrocarbons from carbon monoxide and hydrogen.

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The present invention relates to a process for the activation of a catalyst, in particular to a process for the activation of a catalyst of use in Fischer-Tropsch synthesis.

The preparation of hydrocarbons from a mixture of hydrogen and carbon monoxide at elevated temperature and pressure in the presence of a catalyst is referred to in the literature as the Fischer-Tropsch hydrocarbon synthesis.

Catalysts used in Fischer-Tropsch synthesis typically comprise one or more metals from Group VIII of the Periodic Table, optionally together with one or more promoters, and a support material or carrier. Particular interest exists in Fischer-Tropsch catalysts which comprise cobalt, especially in catalysts comprising cobalt in association with one or more promoters. Cobalt-containing catalysts have found particular application in the Fischer-Tropsch synthesis of hydrocarbons, yielding products consisting virtually completely of unbranched hydrocarbons with a high degree of selectivity to $C_5 +$ hydrocarbons.

Before a catalyst can be used in Fischer-Tropsch synthesis, it must first be activated. Activation is effected by contacting the catalyst with a hydrogen-containing gas. The action of the activation step is to reduce the oxides of the catalytically active metal and oxides of other metals present as promoters in the catalyst. Such activation procedures, applicable to the activation of fresh catalyst and also in the procedures for regenerating or reactivating exhausted catalyst, are known in the art.

Thus, US Patent No. 2,289,731 (US 2,289,731) discloses a process for the reactivation (regeneration) of exhausted Fischer-Tropsch catalysts in which the catalyst is contacted with hydrogen to remove paraffinic hydrocarbons and other deposits from the catalyst particles. US 2,289,731 further discloses that it is of advantage to expose the catalyst particles to the oxidizing action of an oxygen-containing gas prior to being treated with hydrogen.

European Patent Application publication No. 0 168,894 (EP-A-0 168 894) discloses a process for the activation of a cobalt/zirconium/silica catalyst in which the catalyst particles are contacted with a hydrogen-containing gas at a temperature of between 200 and 350 °C and a hydrogen partial pressure between 0.001 and 75 bar, the hydrogen partial pressure being increased gradually or stepwise from an initial value to a final value such that the final value is at least five times the initial value.

US Patent No. 4,670,414 (US 4,670,414) discloses a process for the conversion of synthesis gas into hydrocarbons with a catalyst prepared by subjecting a cobalt carbonyl-impregnated alumina or silica support to an activation procedure comprising the steps, in sequence, of (A) reduction in hydrogen, (B) oxidation in an oxygen-containing gas, and (C) reduction in hydrogen, the activation procedure being conducted at a temperature below 500 °C. The catalyst is preferably slowly reduced in the presence of hydrogen. The reduction step can be conducted initially using a gaseous mixture comprising 5% hydrogen and 95% nitrogen, and thereafter, the concentration of hydrogen can be gradually increased until pure hydrogen is obtained. The reduced catalyst is then passivated at ambient temperature by contact with diluted air, after which the catalyst is slowly heated in diluted air to a temperature of from about 300 °C to about 350 °C. The thus oxidized catalyst is then reduced in the aforementioned manner. A similar activation procedure is disclosed in US Patent No. 4,413,064.

In US 4,670,414 it is stated that the flow of reducing gas during the reduction stages of the procedure must be high enough so that any water formed has a partial pressure in the offgas of below 1%, in order to avoid excessive steaming of the exit end of the catalyst bed. Thus, to keep the water partial pressure to the required low level requires either the provision of equipment capable of handling a high throughput of gas, or operation of the reduction stages at low pressures, in turn requiring longer reduction periods.

Finally, US Patent No. 2,644,829 (US 2,644,829) discloses a process for the start-up or conditioning of a catalyst in a Fischer-Tropsch synthesis process in which, at the start of the synthesis the catalyst is contacted with a mixture of hydrogen and carbon monoxide at a pressure and a gas space velocity substantially lower than the pressure and gas space velocity normally used to effect the synthesis reaction. The pressure and space velocity are then gradually increased until normal process operating conditions are achieved. The effect of this conditioning procedure is described in US 2,644,829 as being to reduce the initial undesirably high level of activity of the catalyst. Thereafter, the synthesis process is continued under normal operating conditions with the catalyst in its state of reduced activity.

It has been found that, during the activation of a Fischer-Tropsch catalyst, the hydrogen-containing gas must be contacted with the catalyst at very high gas space velocities in order to achieve optimum activation. However, the design and construction of commercial scale reactors often places very severe constraints on the maximum permissible pressure drop across a catalyst bed. These constraints in turn mean that the very high gas space velocities desirable during activation cannot be applied without expensive compressor apparatus, if at all. Accordingly, relatively low gas space velocities must be used during activation. This, however, in turn often results in the activation procedures taking many hours to effectively reduce, and hence activate, the catalyst. Therefore, there is a need for an activation procedure

which is capable of effectively activating the catalyst rapidly at low gas space velocities.

Most surprisingly, it has now been found that the operation of an activation procedure for a Fischer-Tropsch catalyst in which the catalyst is reduced by contact with a hydrogen-containing gas under a regime of increasing hydrogen concentration and increasing gas space velocity yields a catalyst having most advantageous properties. In particular, catalysts activated by the aforementioned procedure can exhibit a significantly increased activity and a markedly higher selectivity to $C_5 +$ hydrocarbons than equivalent catalysts activated by means of prior art processes. Further, the aforementioned advantages may be obtained very rapidly by operation at relatively low gas space velocities to meet the pressure drop requirements of commercial plants.

Accordingly, the present invention provides a process for the activation of a Fischer-Tropsch catalyst comprising reducing the catalyst by contact with a hydrogen-containing gas, the hydrogen concentration and the space velocity of the gas contacting the catalyst increasing step-wise or continuously during the activation.

The hydrogen-containing gas used in the process of the present invention may be substantially pure hydrogen gas or a mixture of hydrogen with one or more inert gases, for example nitrogen.

The action of the hydrogen-containing gas on the catalyst during the activation procedure is to reduce oxides of the catalytically active metal, and other metals present. In this respect, the activation of the catalyst by contact with a hydrogen-containing gas to effect the reduction is to be distinguished from the process of contacting the catalyst with a hydrogen-containing gas, such as synthesis gas, to prepare hydrocarbons. The reduction of the metal oxides in the catalyst yields water. As described in US 4,670,414, it is important that the partial pressure of water in the gas contacting the catalyst is kept at a low level, in order to avoid damaging the catalyst. Thus, the water partial pressure in the gas leaving the catalyst bed is preferably maintained at a level below 200 mbar, more preferably below 100 mbar. The maximum water partial pressure possible without damaging the catalyst will vary according to the specific catalyst selected. It having been found that some catalysts are more tolerant to the presence of water than others. When operating with a catalyst having a particularly low tolerance to the presence of water, it may be necessary to maintain the water partial pressure at 50 mbar, or even considerably lower. The tolerance of the catalyst to the presence of water can readily be determined for a given catalyst by determining the activity of the catalyst in Fischer-Tropsch synthesis after contact with varying amounts of water in the activation procedure.

In order to keep the water partial pressure to a minimum, it is preferable to contact the catalyst initially with a hydrogen-containing gas containing a high level of inert gas and, thereafter, increase the hydrogen content of the gas stepwise or continuously whilst monitoring the water content of the gas leaving the catalyst bed. Typically, the catalyst will be initially contacted with a gas containing 0.5% v/v hydrogen or less, the hydrogen content being increased until a hydrogen-rich gas or substantially pure hydrogen is contacting the catalyst.

Thus, a preferred operating regime is to contact the catalyst with an inert gas having a hydrogen content less than 0.5% v/v, most preferably substantially zero, and increasing the hydrogen content of the gas during the activation procedure to a level of from about 70% v/v to about 100% v/v. It is a particular and most surprising advantage of the process of present invention that complete activation of the catalyst can be achieved using a hydrogen-containing gas having a final hydrogen content somewhat less than 100% v/v, for example about 75% v/v. In this way, the need for specialized equipment capable of compressing pure hydrogen gas is obviated.

The flowrate of the hydrogen-containing gas is increased during the process of the present invention from an initial rate at the start of activation process. It is a further advantage of the process of the present invention that lower gas flowrates are needed to effect complete activation of the catalyst than with activation processes of the prior art. Thus, the hourly space velocity of the gas (GHSV) may increase within the range from about 100 to 10000 NI/h during the process, preferably from about 200 to 6000 NI/h . More preferably, the GHSV of the hydrogen-containing gas increases within the range of from 200 to 1500 NI/h . A particularly preferred operating regime for the increasing gas flowrate is to increase the GHSV continuously or stepwise from an initial value of about 300 NI/h to a final value of up to about 1200 NI/h . An especially preferred operating regime is an increase within the range of from 350 NI/h to up to about 1000 NI/h over the duration of the activation process.

The rate at which the flowrate of the hydrogen-containing gas is increased will be determined by the partial pressure of water in the gas leaving the catalyst bed, which in turn is related to the operating pressure of the process and the rate of increase of the hydrogen partial pressure in the gas contacting the catalyst. In general, higher gas hourly space velocities will be required at a given set of operating conditions for activation of catalysts having a high sensitivity to the presence of water. For the activation of more

water-tolerant catalysts, lower gas space velocities and/or higher hydrogen concentrations can be employed.

The activation process of the present invention is carried out at an elevated temperature, preferably below 500 °C. More preferably, the process is operated at a temperature of from 100 °C to 350 °C, especially in the range of from 200 to 300 °C. A preferred temperature for operation of the process is about 250 °C. Conveniently, the temperature is maintained at a constant level throughout the activation procedure. Alternatively, the temperature may be increased stepwise or continuously during the activation, for example from an initial value of 100 °C to a final value of up to 350 °C. More preferably, the temperature is increased within the range of from 200 to 300 °C.

The activation process of the present invention is operated at elevated pressure, typically from about 1 to 30 bar, preferably from about 1 to 10 bar. More preferably, the catalyst is contacted with the hydrogen-containing gas at a pressure in the range of from 2 to 8 bar. It will be appreciated that the higher the operating pressure, the higher the partial pressure of any water present in the gas leaving the catalyst bed. An operating pressure of from about 3 to 6 bar is particularly preferred. It is preferred that the pressure of the hydrogen-containing gas contacting the catalyst is maintained substantially constant throughout the activation process.

The length of time that the catalyst is subjected to the activation process will again depend upon the precise operating conditions and the degree of reduction required, as indicated by the water content of the gas leaving the catalyst bed; a low water content indicating that a high degree of reduction has been achieved. Typically, the process is operated for a period of from about 1 to 50 hours, more preferably from about 5 to 25 hours.

The process of the present invention may be applied to activate a fresh catalyst, prior to its use in a Fischer-Tropsch synthesis. Alternatively, the process may be applied in the regeneration (reactivation) of an exhausted or partially exhausted catalyst. In this respect, the term "activation" as used herein is to be taken as a reference to the activation of a fresh catalyst prior to its use and to the regeneration (reactivation) of an exhausted or partially exhausted catalyst.

Further, the process of the present invention may be advantageously applied in the reduction/oxidation/reduction, or the so-called "ROR-activation" procedure described in US 4,670,414. The ROR-activation procedure may be advantageously applied in the activation of a fresh catalyst prior to its use, or in the regeneration (reactivation) of an exhausted or partially exhausted catalyst.

Thus, according to a further aspect of the present invention, there is provided a process for the activation of a Fischer-Tropsch catalyst comprising the steps of a) contacting the catalyst with a hydrogen-containing gas; b) contacting the catalyst with a gas having oxidizing activity; and c) contacting the catalyst with a hydrogen-containing gas; characterized in that a process as hereinbefore described is employed in at least one of steps a) and c).

Either one or both of the reduction stages in the ROR-activation procedure may comprise the process of the present invention. If the process is employed during only one of the reduction stages of the ROR-activation procedure, it is most preferably used during the second reduction stage.

In the first stage in the ROR-activation procedure, the catalyst particles are contacted with a hydrogen-containing gas. The process as hereinbefore described may be employed as the first stage in the ROR-activation procedure.

Alternatively, a known reduction procedure may be used, such as described in US 4,670,414. The hydrogen-containing gas used in such a procedure may be substantially pure hydrogen or may comprise hydrogen diluted by one or more inert gases, such as nitrogen. The hydrogen-containing gas may be supplied at a pressure of from 1 to 30 bar, for example about 25 bar. The catalyst is preferably contacted with the gas at a temperature below 500 °C, preferably at a temperature of from 100 to 400 °C, typically from 150 to 350 °C and at a GHSV of from 100 to 10000 NI/l/h, more preferably from 200 to 6000 NI/l/h, for a period of from 1 to 50 hours.

The second stage of the ROR-activation procedure is an oxidation stage, in which the catalyst is contacted with a gas having an oxidizing action. The gas used in this stage is conveniently oxygen or an oxygen-containing gas, for example air. The reactions occurring during the oxidation stage are exothermic. In order to avoid an excessive rise in temperature which could damage the catalyst, it is preferred to contact the catalyst with air, further diluted with nitrogen. Typically the gas contains from about 1 to 5% v/v, preferably about 3% v/v oxygen. The temperature at which the oxidation is effected is in the range of from 100 to 400 °C, preferably from 150 to 350 °C. The catalyst is contacted with the oxygen-containing gas at a pressure of from 1 to 25 bar, typically about 10 bar, at a GHSV of from about 100 to 5000 NI/l/h, typically from 500 to 1000 NI/l/h, for a period of from 1 to 30 hours.

The third stage of the ROR-activation procedure is a final reduction of the oxidized catalyst produced in the second stage described above. For this third stage, if the process of the present invention, as hereinbefore described, has been employed in the first stage of the ROR-activation, the known reduction process described above in relation to the first stage may be employed. Most preferably, the process of the present invention is employed in the third stage of the ROR-activation procedure.

In a further aspect, the present invention provides a Fischer-Tropsch catalyst whenever activated by a process as hereinbefore described.

The process of the present invention may be applied as a one-pass process, that is, a process in which the hydrogen-containing gas fed to the catalyst bed contacts the catalyst only once. In a preferred embodiment, the gas leaving the catalyst bed is dried to reduce the water content of the gas, recompressed to the process operating pressure and recycled to the inlet for the catalyst bed. In a particularly preferred embodiment, the dried, hydrogen-containing gas being recycled, together with the fresh, hydrogen-containing feed gas, is heated by recovering heat from the gas leaving the catalyst bed.

The process of the present invention will be further described with reference to the accompanying figure which is a schematical diagram of a preferred arrangement of apparatus for conducting the process of the present invention.

Referring to the Figure, a reactor vessel 2 has an inlet line 8 and an outlet line 10. Advantageously, fresh catalyst is loaded into a catalyst bed within the reactor 2 prior to being activated by the process of the present invention. The catalyst may also be regenerated (reactivated) whilst remaining in the reactor vessel 2. The catalyst may be regenerated (reactivated) several times whilst remaining in the reactor vessel 2, throughout its useful life.

During the process of the present invention, hydrogen-containing feed gas enters the reactor vessel 2 from the inlet line 8 and contacts the catalyst bed. Effluent gas exiting the catalyst bed leaves the reactor vessel 2 and enters the outlet line 10. The effluent gas in the outlet line 10 is depleted in hydrogen and is rich in water-vapour, relative to the feed gas in the inlet line 8. From the outlet line 10, the effluent gas flows to a feed/effluent heat exchanger 16 to undergo a first stage of cooling and then, via line 14, to a further cooler 18 to undergo a second stage of cooling in preparation for compression. The effluent gas leaves the cooler 18 and, through line 20, enters a suction knock-out drum 22. In the suction knock-out drum 22, water, now present as droplets entrained in the effluent gas, is removed from the effluent gas stream and leaves the suction knock-out drum 22 through line 24. From the suction knock-out drum 22, the effluent gas is fed, via line 26, to the inlet of a compressor 28. The compressed effluent gas leaves the compressor 28 via line 30, is cooled in a discharge cooler 32 and fed, via line 34, to a discharge knock-out drum 36. The action of compression and cooling on the effluent gas stream causes further droplets of water to form, which collect and are removed from the discharge knock-out drum 36 through line 38. From the discharge knock-out drum 36, the effluent gas is mixed with fresh hydrogen-containing gas from line 40 and the combined gas stream fed, through line 42, to a molecular sieve dryer 44.

The molecular sieve dryer 44 may typically contain an aluminosilicate adsorbant for removing water from the combined gas stream. Water is shown, schematically, leaving the molecular sieve dryer 44 through line 46 and the dried gas stream is shown leaving through line 48.

The dried gas stream is heated by heat exchange with the effluent gas leaving the reactor 2 in the feed/effluent exchanger 16. From the feed/effluent exchanger 16, the gas stream is fed, via line 50, to a trim heater 52 to bring the gas up to the process operating temperature. The hot gas enters the reactor 2 from the trim heater 52 through line 8.

The apparatus represented in the Figure may be used to service a plurality of reactor vessels (not shown), each of which is isolated by valves and which may, in turn, be connected to the process apparatus shown in the Figure for activation or regeneration (reactivation) of the catalyst therein.

A bypass line (not shown) may be provided between the two lines 8, 10 to allow gas to bypass the reactor vessel 2 and be removed from the process apparatus as a purge.

The process of the present invention may be applied to any Fischer-Tropsch catalyst. Fischer-Tropsch catalysts frequently comprise, as the catalytically active component, a metal from Group VIII of the Periodic Table of Elements. Particular catalytically active metals include iron, cobalt and nickel. The process of the present invention is particularly advantageous when applied to Fischer-Tropsch catalysts comprising cobalt as the catalytically active metal.

The catalytically active metal is preferably supported on a porous carrier. The porous carrier may be selected from any suitable refractory metal oxide or silicates or a combination thereof. Particular examples of preferred carriers include silica, alumina, titania or mixtures thereof. Most preferably, a porous silica carrier is used. The active metal may be applied to the carrier by any of the techniques well known in the art, for example kneading, impregnation or precipitation. Impregnation is a particularly preferred technique.

which may be carried out by contacting the carrier with a compound of the active metal in the presence of a liquid, most conveniently in the form of a solution of the metal compound. The compound of the active metal may be inorganic or organic. Inorganic compounds of the active metal are preferred, in particular nitrates. The liquid used may also be either organic or inorganic, with water being a particularly preferred and convenient liquid.

The amount of catalytically active metal on the carrier is preferably from 3 to 100 pbw per 100 pbw of carrier material, more preferably from 10 to 80 pbw, especially from 20 to 60 pbw.

If desired, the catalyst may also comprise one or more metals or metal oxides as promoters. Suitable metal oxide promoters may be selected from groups IIa, IIb, IVb, Vb and VIb of the Periodic Table, or the actinides and lanthanides. In particular, oxides of magnesium, calcium, strontium, barium, scandium, yttrium, lanthanum, cerium, titanium, zirconium, hafnium, thorium, uranium, vanadium and chromium are most suitable. A particularly preferred metal oxide promoter is zirconium oxide. Suitable metal promoters may be selected from groups VIIb or VIII of the Periodic Table. Rhenium and group VIII noble metals are particularly suitable, with ruthenium, platinum and palladium being especially preferred. The promoter may be applied to the porous carrier either before or after application of the catalytically active metal. The amount of promoter present is preferably from 0.1 to 150 pbw per 100 pbw of carrier. A particularly preferred catalyst is a cobalt/zirconium/silica catalyst.

Examples of suitable catalysts to which the process of the present invention may be applied are disclosed in European Patent Applications publication Nos. EP 0 104 672, EP 0 110 449, EP 0 127 220, EP 0 167 215, EP 0 180 269 and EP 0 221 598. Examples of very suitable processes for preparing such catalysts are disclosed in UK patent applications Nos. GB 8918845.2 and GB 8925979.0, forming priority for published European patent application publication Nos. EP 0 421 502 and EP 0 428 223 respectively.

The Fischer-Tropsch catalyst, once activated by the process of the present invention is suitable for use in a process for the synthesis of hydrocarbons from a mixture of carbon monoxide and hydrogen, which mixture is commonly referred to as synthesis gas. The conversion of the mixture of hydrogen and carbon monoxide may be carried out at a temperature of from about 125 to about 350 °C, preferably from about 175 to 250 °C, and at a pressure of from about 5 to 100 bar, more preferably from about 10 to 50 bar. In the process, the catalyst may be contacted with a synthesis gas having a hydrogen to carbon monoxide molar ratio less than 2.5, preferably less than 1.75. More preferably, the hydrogen to carbon monoxide molar ratio of the synthesis gas is in the range of from 0.4 to 1.5, especially from 0.9 to 1.3.

The process of the present invention is further illustrated by the following examples, in which Examples 2 to 5 are activation procedures according to the present invention and Examples 6 to 10 are activation procedures known from the prior art and are for comparative purposes only.

35 Example 1 - Catalyst Preparation

Silica spheres (Grade HT-89; 1.5 mm nominal diameter) were loaded into a reactor vessel and dried by contact with nitrogen at a pressure of 4.5 bar whilst heating at a rate of 50 °C/hr to a final temperature of 200 °C. The spheres remained under these final conditions for 2 hours and were subsequently cooled to a temperature below 50 °C. A zirconium-containing solution ($\text{Zr}(\text{OC}_3\text{H}_7)_4$, 41.7% by weight; n-propanol, 13.9% by weight; acetyl-acetone, 23.3% by weight; toluene, 21.1% by weight) was pumped into the reactor and circulated over the silica spheres for a period of 1.5 hours to allow the bed to reach equilibrium. The reactor was then drained of the solution and the silica spheres flushed with nitrogen at room temperature (20 °C). The solvent remaining in and around the silica spheres was evaporated by heating the spheres to a final temperature of 200 °C in nitrogen at a rate of 50 °C/hr. The spheres were held under these final conditions for 14 hours. After this time, the temperature was again increased, at a rate of 50 °C/hr, to a final temperature of 500 °C and the spheres maintained at this temperature, in an atmosphere of nitrogen, for a period of 1 hour. A mixture of oxygen in nitrogen (0.5 %v O_2) was admitted and the silica spheres held under these conditions for 7 hours. Thereafter, the temperature was increased to 600 °C and the oxygen concentration gradually increased to 2.5 %v for a period of 5 hours. After this time, the spheres were allowed to cool to room temperature.

An aqueous solution of cobalt nitrate ($\text{Co}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$) having a cobalt concentration of 17.7% by weight was prepared and heated to a temperature of from 60 to 70 °C. The silica spheres prepared above were heated to a temperature of from 90 to 100 °C and immersed in the solution for a period of 30 minutes. The silica spheres were then dried in air at 60 to 70 °C for 7 hours and thereafter calcined by heating at a rate of 35 °C/hr to a temperature of 500 °C, finally being held at this temperature for 1 hour prior to cooling to room temperature.

The resulting catalyst comprised 7.27% by weight zirconium and 17.6% by weight cobalt.

Examples 2 to 5 - Catalyst Activation and Testing

Four samples of the catalyst prepared in Example 1 were each loaded into a fixed bed reactor and subjected to an activation procedure according to the present invention. The conditions and duration of the activation for each sample are given in Table I. In each activation procedure the conditions were varied so as to maintain a water partial pressure in the off-gas leaving the reactor of below about 50 mbar. The ranges given in Table I for temperature, gas hourly space velocity (GHSV) and hydrogen concentration indicate the starting point and end point for that parameter, the parameter being increased continuously throughout the duration of the activation. The hydrogen gas fed to the reactor in each case was diluted with nitrogen to the indicated hydrogen concentration.

Once activated, each of the catalyst samples was subjected to a hydrocarbon synthesis test, in which the catalyst was contacted with a mixture of carbon monoxide and hydrogen, having a hydrogen/carbon monoxide ratio of about 1.1, at a GHSV of 800 NL/h at a pressure of 26 bars. The operating temperature of the reactor, space time yield (STY) and selectivity to C_5 hydrocarbons and larger ($\text{C}_5 +$ selectivity) achieved in each of the tests are given in Table II.

Comparative Examples 6 to 10

For comparative purposes, five further samples of the catalyst prepared in Example 1 were activated according to procedures known from the prior art. The conditions during activation of the five comparative examples were as described above for Examples 2 to 5, with the exception of those parameters as indicated in Table I.

The five activated catalyst samples were then each subjected to a hydrocarbon synthesis test under the same conditions as described above with reference to Examples 2 to 5. The results of these tests are set out in Table II.

Table I

Example No.	2	3	4	5	6	7	8	9	10
Pressure (bar)	5	5	5	5	3	5	5	3	3
Duration (hours)	50	48	50	50	5	55	75	20	70
GHSV (NL/l/h)	400→600	400→600	400→600	350→500	6000	400	250	600	600
Hydrogen Con- centration (%v)	1→75	1→75	1→75	1→75	1→50	1→50	1→50	100	1→100
Temperature (°C)	240→260	240→260	260	240→260	260	240	240	180→260	200→260

Table II

Example No.	2	3	4	5	6	7	8	9	10
Temperature (°C)	216	216	219	216	213	220	220	227	210
Duration (hours)	100	300	800	400	300	100	150	300	100
STY (gC ₅ +/l/h)	97	94	99	110	96	95	96	88	103
C ₅ + selectivity (%w)	91	90	88.5	90	88	88.5	90	88.5	87

From the data set out in Table II, it can be seen that, in general, a catalyst activated using a procedure according to the present invention (Examples 2 to 5) exhibits an excellent overall activity (as indicated by a low synthesis temperature) giving high space time yields with a very high selectivity to C₅ + hydrocarbons.

From a comparison of the performance of the catalyst activated by procedures according to the present invention with the same catalyst activated following procedures known from the prior art (Examples 6 to 10),

the following will be realized:

As shown in Example 6, a very high gas space velocity during activation yielded a catalyst having an excellent activity (low synthesis temperature), a high yield and a very high C₅ + selectivity. This high level of catalyst performance was achieved at gas space velocities of no more than 10% the value used in Example 6 by applying the process of the present invention. By comparison, activation using a constant gas space velocity of 10% or less than that of Example 6 (Examples 7 to 10) yielded a catalyst having a significantly lower yield, activity and selectivity.

Further, in general the activation procedure of the present invention required considerably less time to achieve a high degree of catalyst activation than equivalent processes of the prior art.

Finally, as shown in Tables I and II, the activation procedure of the present invention did not require the use of pure hydrogen to achieve a high degree of catalyst activation.

Claims

1. A process for the activation of a Fisher-Tropsch catalyst comprising reducing the catalyst by contact with a hydrogen-containing gas, the hydrogen concentration and the space velocity of the gas contacting the catalyst increasing step-wise or continuously during the activation.
2. A process according to claim 1, wherein the hydrogen-containing gas comprises an inert gas.
3. A process according to either of claims 1 or 2, wherein the water partial pressure in the gas leaving the catalyst is maintained below 200 mbar, preferably below 100 mbar.
4. A process according to any preceding claim, wherein the hydrogen content of the hydrogen-containing gas is increased from about 0 to about 75% v/v during the activation.
5. A process according to any preceding claim, wherein the space velocity is increased within the range of from 100 to 10000 NI/h, preferably within the range of from 200 to 6000 NI/h, more preferably within the range of from about 300 NI/h up to about 1000 NI/h.
6. A process according to any preceding claim, wherein the pressure of the hydrogen-containing gas is substantially constant during the activation.
7. A process according to any preceding claim, wherein the pressure of the hydrogen-containing gas is in the range of from 1 to 10 bar.
8. A process according to any preceding claim, wherein the activation is effected at a temperature in the range of from 100 to 350 °C.
9. A process according to any preceding claim, wherein the gas leaving the catalyst is dried, combined with fresh hydrogen-containing gas and recycled to further contact the catalyst.
10. A process for the activation of a Fischer-Tropsch catalyst comprising the steps of:
 - a) contacting the catalyst with a hydrogen-containing gas;
 - b) contacting the catalyst with a gas having oxidizing activity; and
 - c) contacting the catalyst with a hydrogen-containing gas, wherein a process as defined in any one of claims 1 to 12 is employed in at least one of steps a) and c), preferably in at least step c).
11. A process according to any preceding claim, characterized in that the catalyst comprises silica, alumina, titania or mixtures thereof as carrier.
12. A process according to any preceding claim, characterized in that the catalyst comprises cobalt as a catalytically active metal.
13. A process according to any preceding claim, characterized in that the catalyst comprises, as promoter, zirconium.
14. A Fischer-Tropsch catalyst activated by a process according to any preceding claim.

15. A process for the preparation of hydrocarbons comprising contacting a mixture of carbon monoxide and hydrogen with a catalyst according to claim 14.

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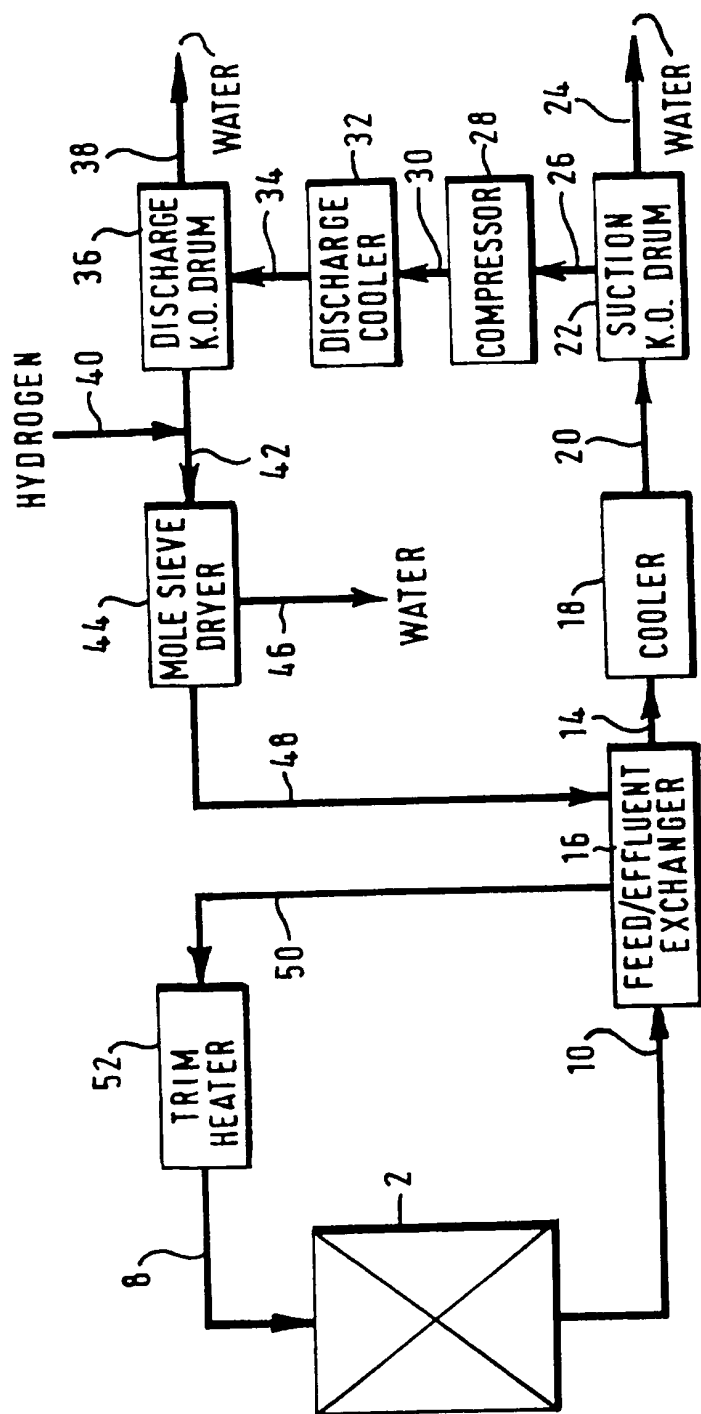
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European Patent
Office

EUROPEAN SEARCH REPORT

Application Number

EP 92 20 2516

DOCUMENTS CONSIDERED TO BE RELEVANT			
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int. Cl.5)
D,A	EP-A-0 168 894 (SHELL) * claims 1,3,4,9,10 * ---	1,7,8, 11,12, 13,14,15	C07C1/04 C10G2/00 B01J37/18
A	EP-A-0 152 652 (SHELL) * claims 1,3,4,5 * * page 2, line 23 - line 27 * * tables II,III * ---	1,7,8, 11,12, 13,14,15	
P,A	WO-A-9 206 784 (EXXON) * claims 1,2,3,4,6,10 * * page 6, line 28 - line 35 * ---	1,2,3, 11,12,13	
A	US-A-4 492 774 (GULF) * claim 1 * ---	1,10,12	
D,A	US-A-2 644 829 (PHILLIPS PETROLEUM) * claims 1,2,4,5,6 * * column 2, line 38 - line 40 * ---	1,5,8, 12,14,15	TECHNICAL FIELDS SEARCHED (Int. Cl.5)
D,A	US-A-4 670 414 (KOBYLINSKI) * claims 1,2,3,4 * -----	1,10	C07C C10G B01J
The present search report has been drawn up for all claims			
Place of search THE HAGUE		Date of completion of the search 01 DECEMBER 1992	Examiner OSWALD DE HERDT
CATEGORY OF CITED DOCUMENTS		T : theory or principle underlying the invention E : earlier patent document, but published on, or after the filing date D : document cited in the application L : document cited for other reasons ----- & : member of the same patent family, corresponding document	
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